



**THE CHOICE OF WORKING FLUID:**  
**THE MOST IMPORTANT STEP FOR A SUCCESSFUL**  
**ORGANIC RANKINE CYCLE**  
**(AND AN EFFICIENT TURBINE)**

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## The key messages of this lecture

- the choice of the **working fluid** is the most relevant degree of freedom in the design of ORC
- The **turbine** is the most critical component of ORC, it plays a fundamental role in system performance, as well as in system cost
- There is a strong relationship between the working fluid properties and the turbine architecture (speed of revolution, number of stages, dimensions) and performance (isentropic efficiency)
- The **working fluid** selection must account for its consequences on the **turbine** design
- There are several peculiarities of ORC turbines, if compared to conventional (gas, steam) turbines:
  - The overall specific expansion work (kJ/kg) is much lower: it can be handled in **few stages**, at relatively **low peripheral speeds**
  - The adoption of **transonic/supersonic** flows is generally mandatory
  - A **large variety** of solutions (axial or radial inflow single stage, multi-stage axial, outflow or mixed radial/axial) can be adopted



## Outline of the lecture

- Brief summary of working fluid selection criteria
  - General characteristics
  - The most relevant thermodynamic properties
  - Power cycle configurations
- The most important parameters affecting the turbine efficiency:
  - Stage specific speed
  - Volume ratio
  - Size parameter
- A **new general correlation** for preliminary (but quite accurate!) prediction of the turbine isentropic efficiency
- Some examples of ORC turbines successfully designed in the last **35 (!) years**



## General (evident) criteria for working fluid selection

The working fluid should be:

*Requirements shared with the refrigerating and air-conditioning industry*

- commercially available (low specific cost, large quantity)
- Non-flammable
- Non-toxic
- environmental benign (low ODP, low GWP)
- compatible with materials (elastomers, metals,...)
- .....
- .....

*A specific requirement for ORC*

- thermally stable

Some of the above requirements may not be fulfilled, especially for high temperature applications



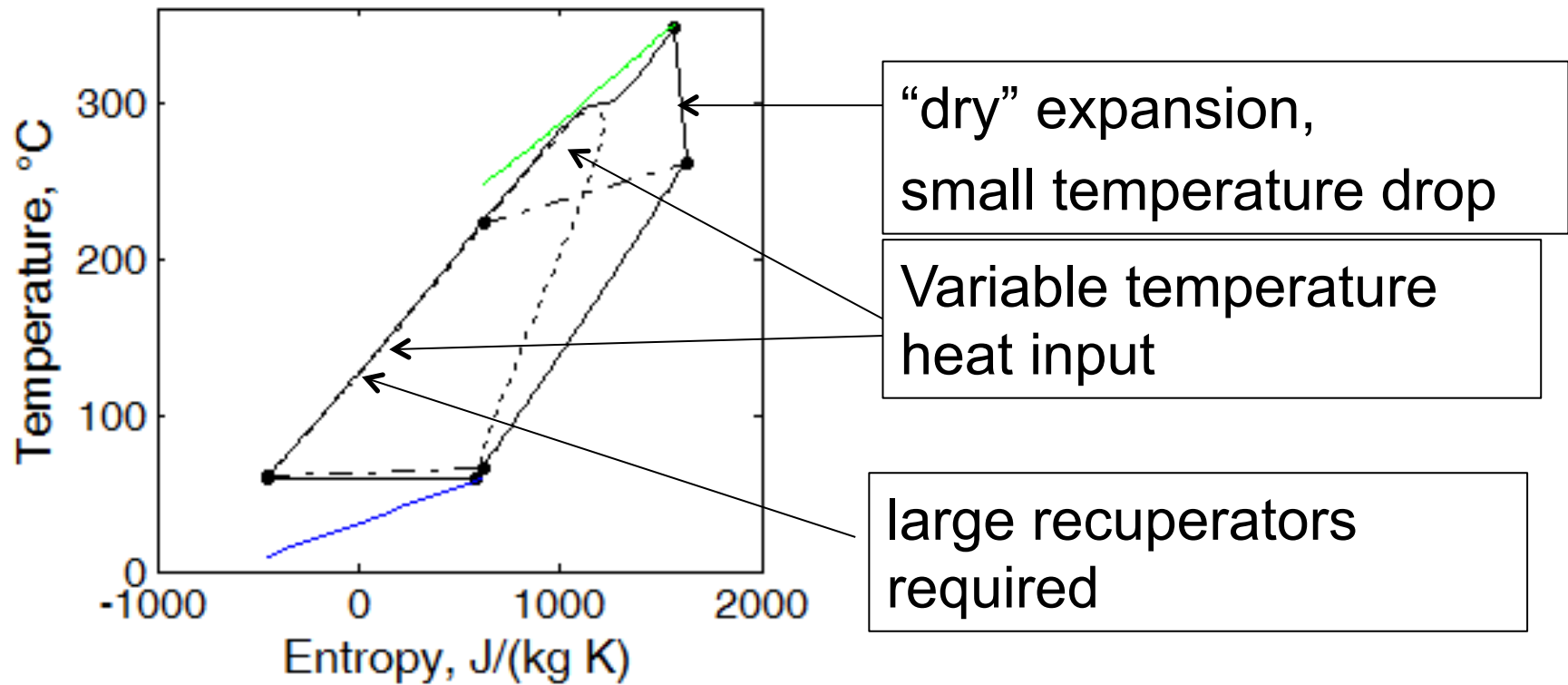
## Thermodynamic criteria for working fluid selection

Relevant properties:

- Molecular complexity (number of atoms per molecule): influences the “shape” of the Andrews curve and power cycle. Complex molecules cause:
  - “dry” expansion 😊
  - large fractions of heat input at variable temperature 😊
  - small temperature drops in the expansion phase 😞
  - large recuperators required 😞



## Supercritical cycle with highly complex working fluid





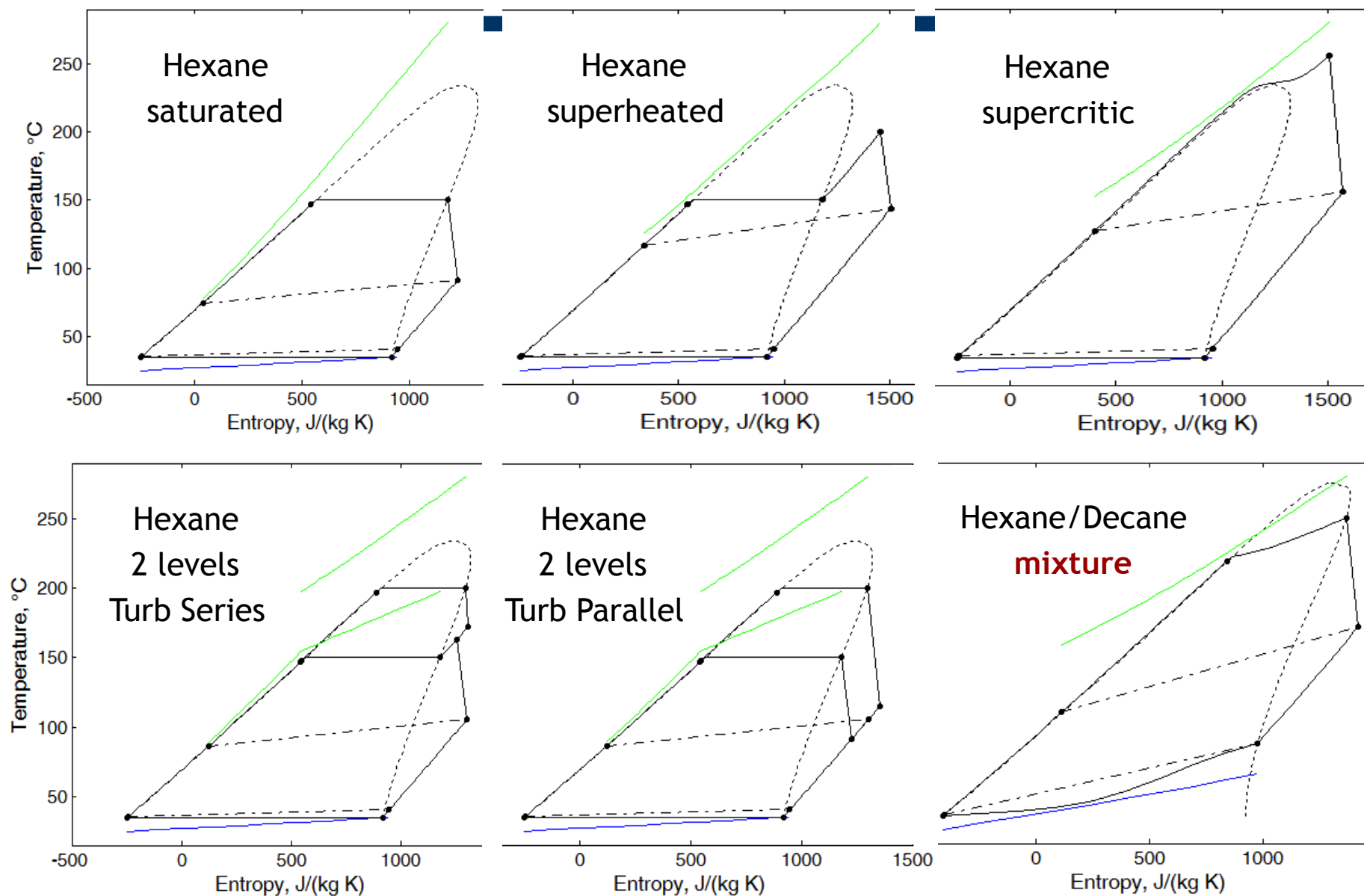
# Thermodynamic criteria for working fluid selection

## Relevant properties:

- Molecular complexity (number of atoms/molecule): influences the “shape” of the power cycle.
- Molecular mass. **Heavy** molecules cause:
  - small enthalpy drop during expansion 😊 😊
  - poor heat transfer coefficients 😞
- Critical temperature:
  - fundamental choice to **match the heat source and sink characteristics**
  - condensation pressure: **relevant** for dimensions (and cost) of turbine and heat exchangers
- Pure fluid or mixture??
  - the presence of a **glide** (evaporation and condensation at variable temperature) could be advantageous for variable temperature heat sources and sinks



# A large variety of cycle configurations







# Turbine Design

- According to similarity rules, the efficiency of a turbine stage is primarily set by its **specific speed** and **specific diameter**

$$N_s = \frac{RPS}{\sqrt{\dot{V}_{out, is} / \Delta h_{is}}} \sqrt[3]{\frac{1}{4}}$$

$$D_s = \frac{D_m}{\sqrt{\dot{V}_{out, is} / \Delta h_{is}}} \sqrt[1]{\frac{1}{4}}$$

- Other parameters, relevant for the turbine efficiency, are the **volume ratio** (compressibility effects) and the **size parameter** (dimensional effects: thickness, clearance, roughness, etc.)

$$V_{ratio} = \frac{\dot{V}_{out, is}}{\dot{V}_{in}}$$

$$SP = \frac{\sqrt{\dot{V}_{out, is}}}{\Delta h_{is}^{1/4}}$$

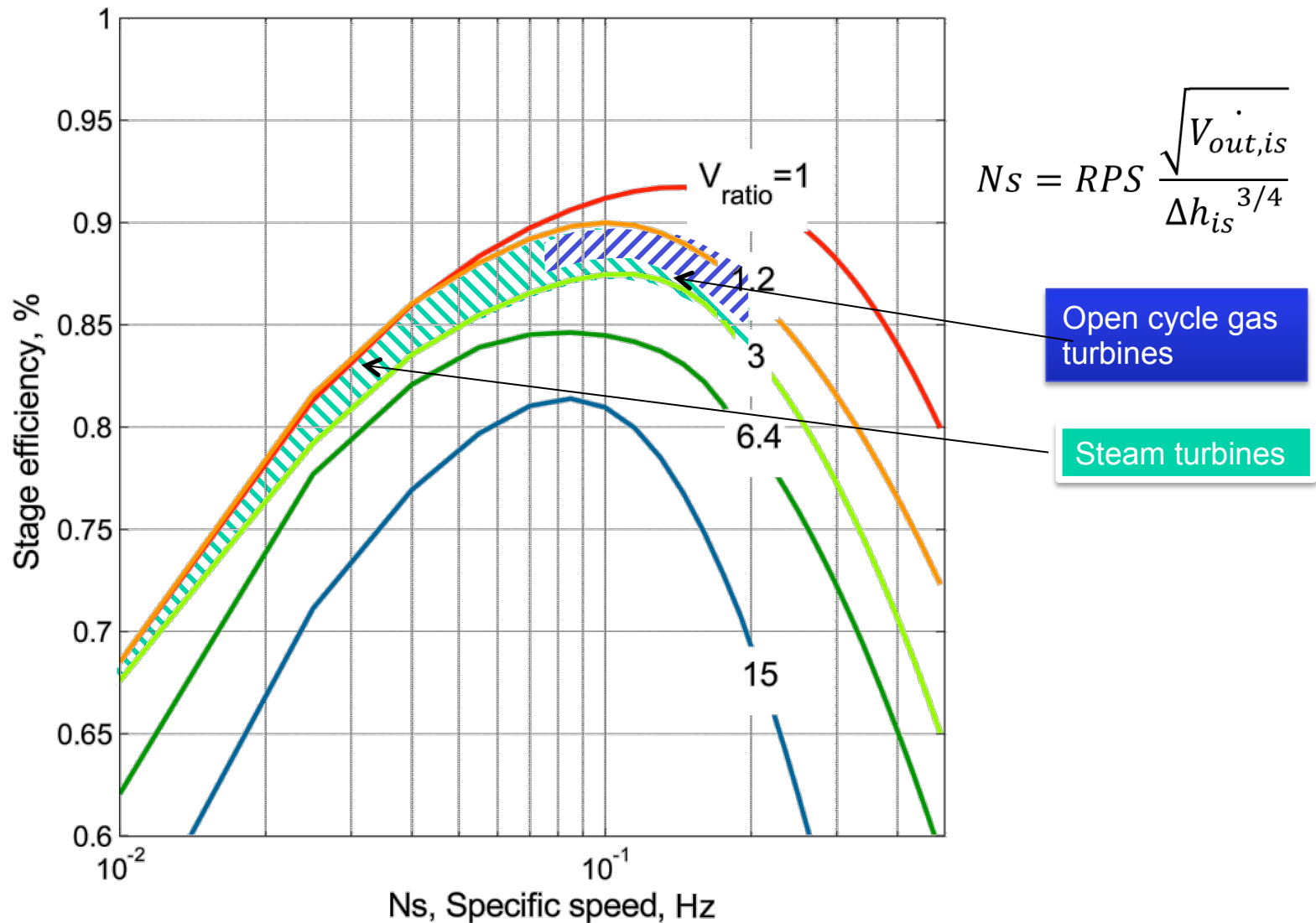


## Turbine Design

- Both **open-cycle gas turbines** and **steam turbines** are characterized by **large enthalpy drops** (air and steam have **light molecules**):
  - **multi-stage** turbines are required
  - the expansion ratio/stage is **relatively small**
- In **open-cycle heavy-duty** gas turbines the volumetric flow rate experiences moderate variations along the expansion, so nearly optimum  $N_s$  can be adopted in all stages
- In steam cycles, the variation of volumetric flow rate is dramatic: single-shaft solutions must deal with non-optimum  $N_s$  (too low in HP, too high in LP)
- **ORC turbines** are characterized by **heavy** molecules, **small enthalpy drops**.



# Important parameters in turbine design: specific speed





# Turbine Design

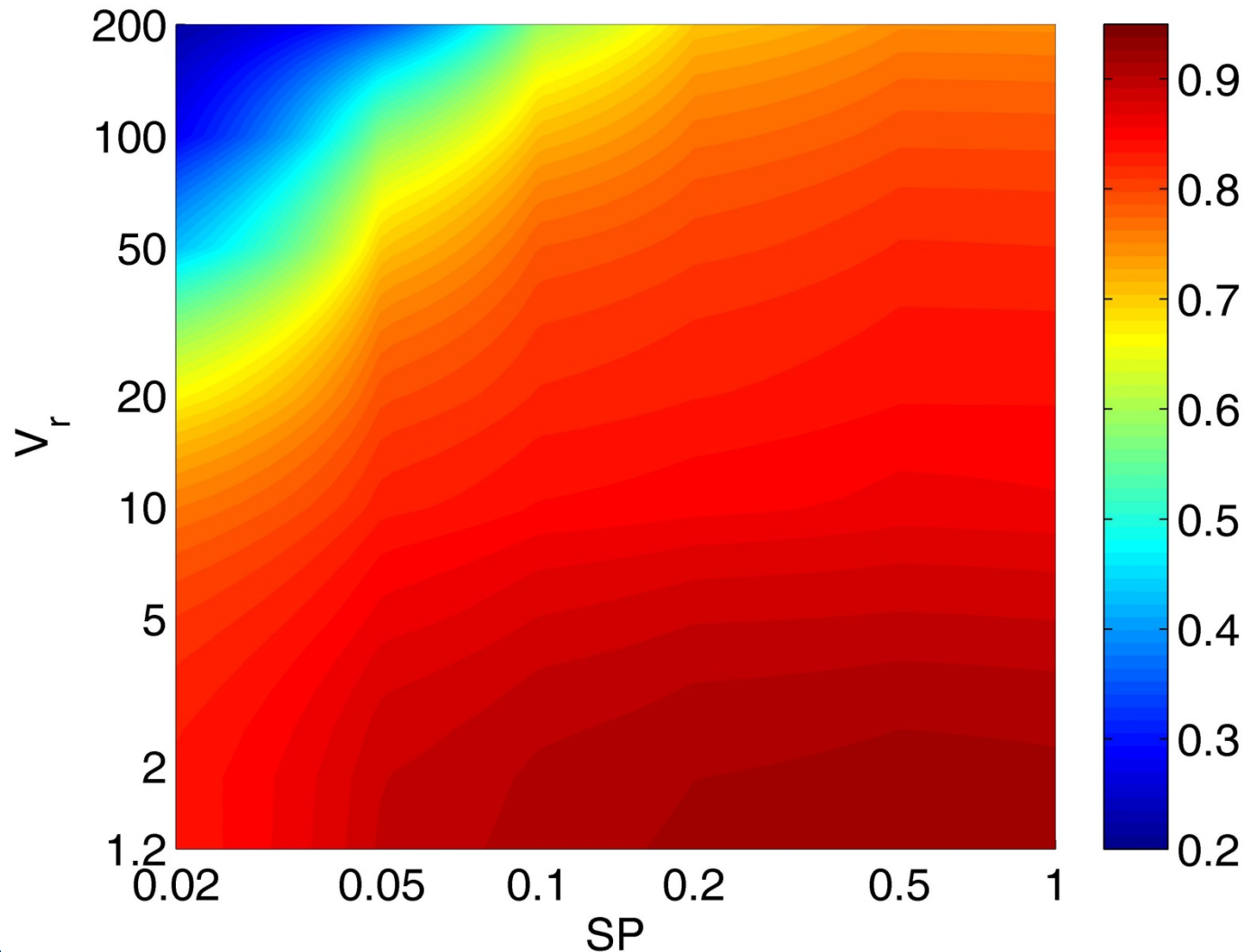
ORC turbines are characterized by:

- heavy molecules → small enthalpy drops → few stages → large  $V_r$  per stage relevant compressibility effects (supersonic flows)
- large overall  $V_r$  → large blade height variation in multi-stage turbines
- The possibility of:
  - designing the turbine at optimum values of  $N_s$  and  $D_s$
  - obtaining a proper SP by selecting the working fluid properties (most relevant one : condensing pressure)

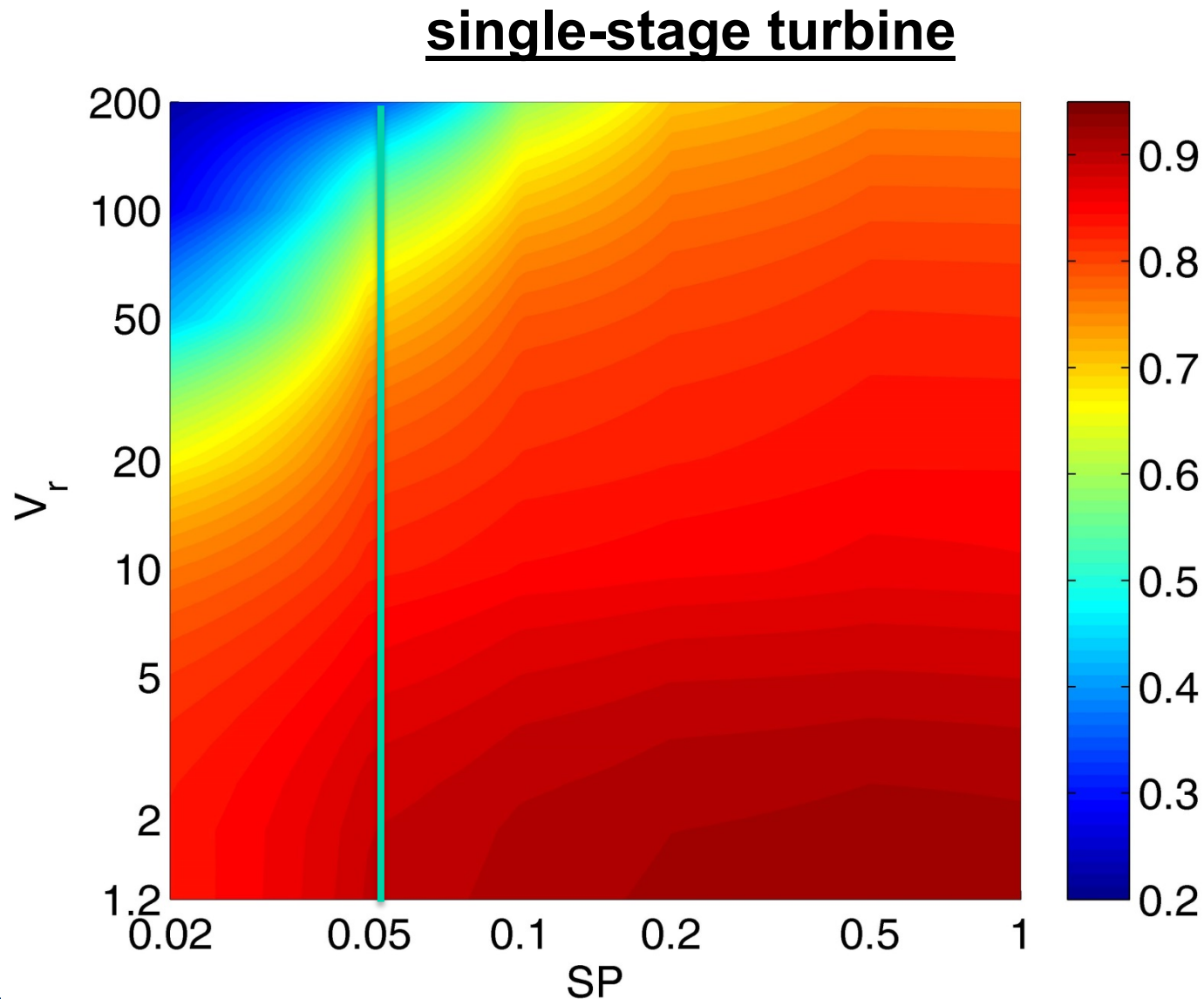


A new efficiency prediction map based on both **Vr** and **SP**, for optimized **Ns**, **Ds**

### single-stage turbine

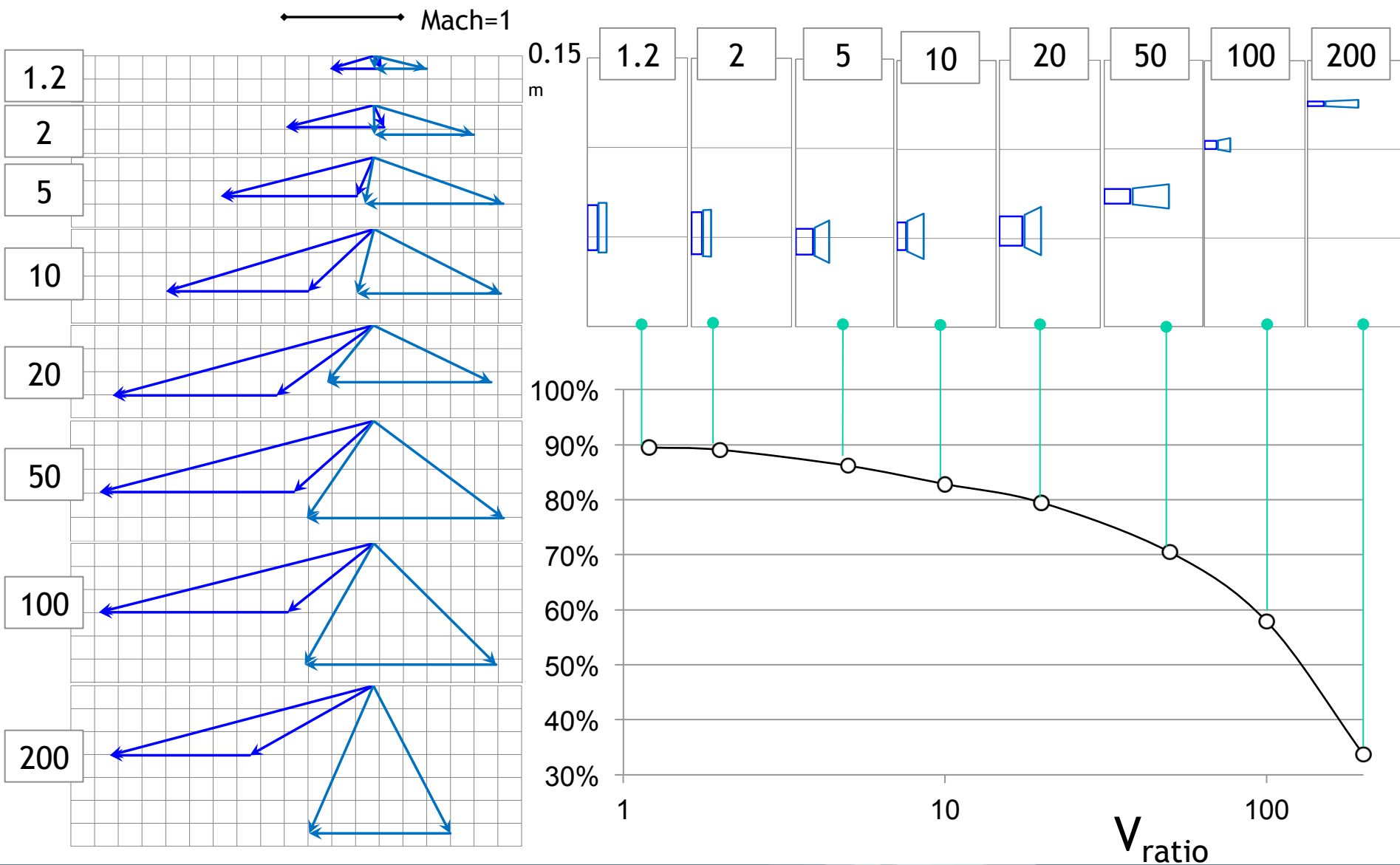


# ↘ The influence of $V_r$





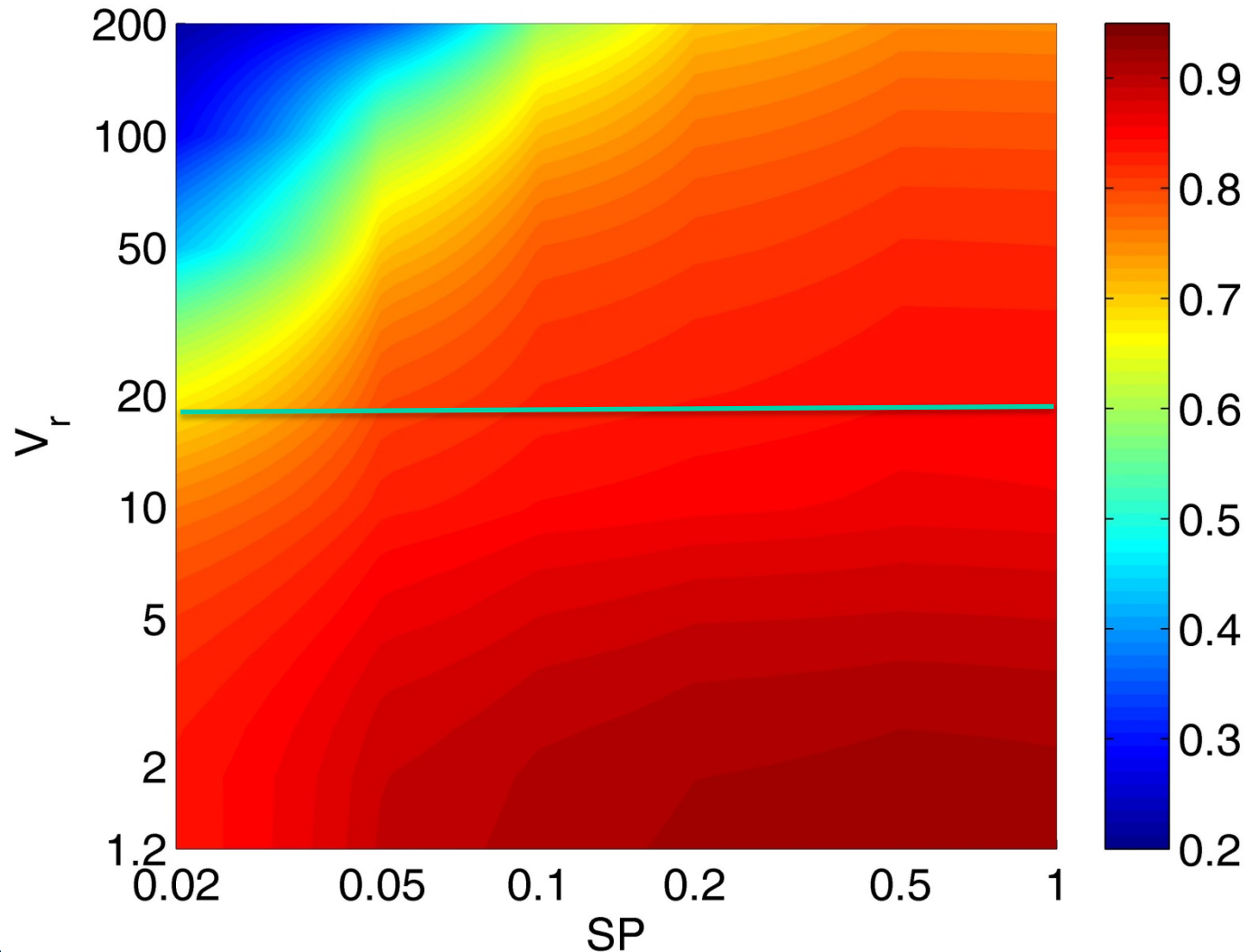
# The influence of $V_r$





# The influence of SP

## single-stage turbine

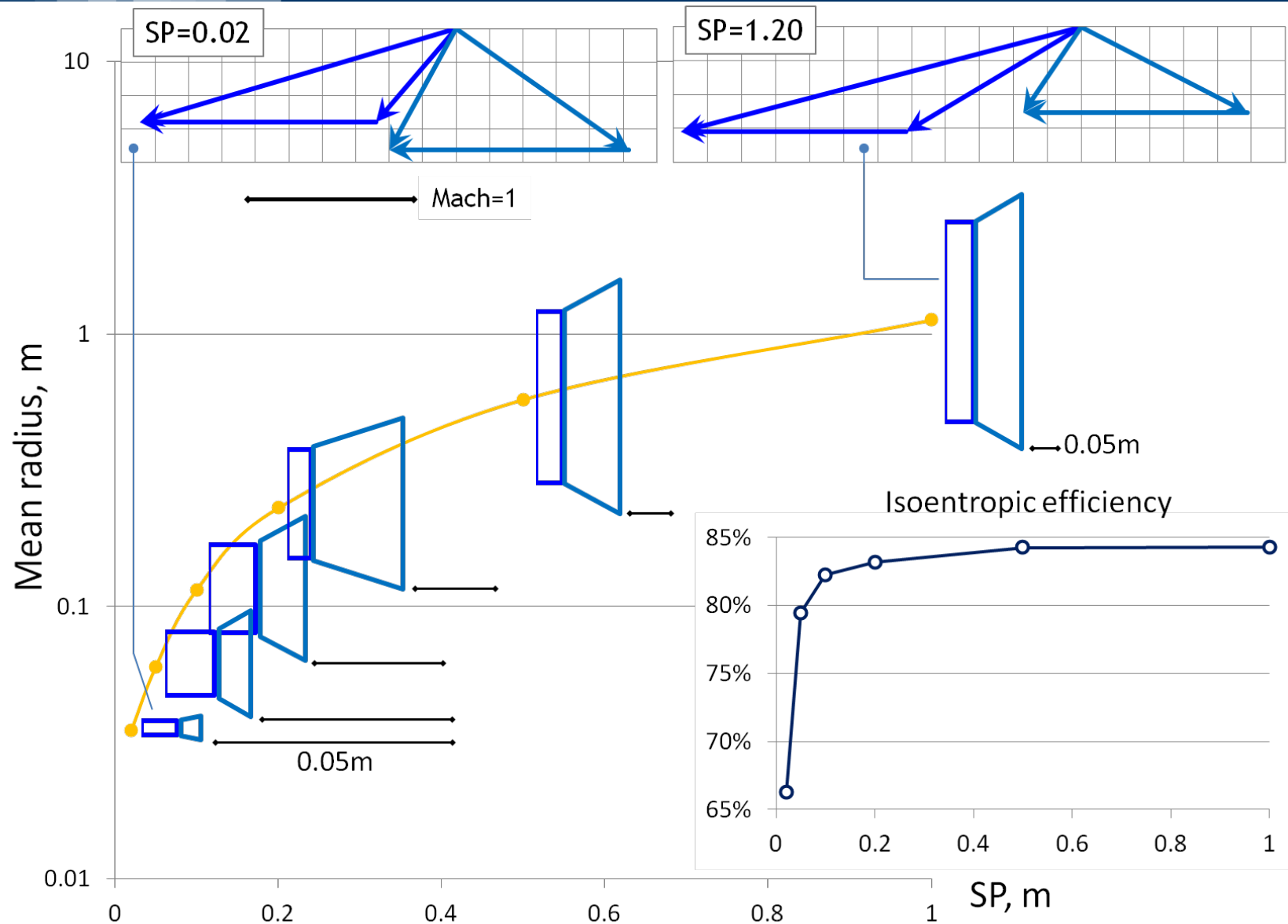






# The influence of SP

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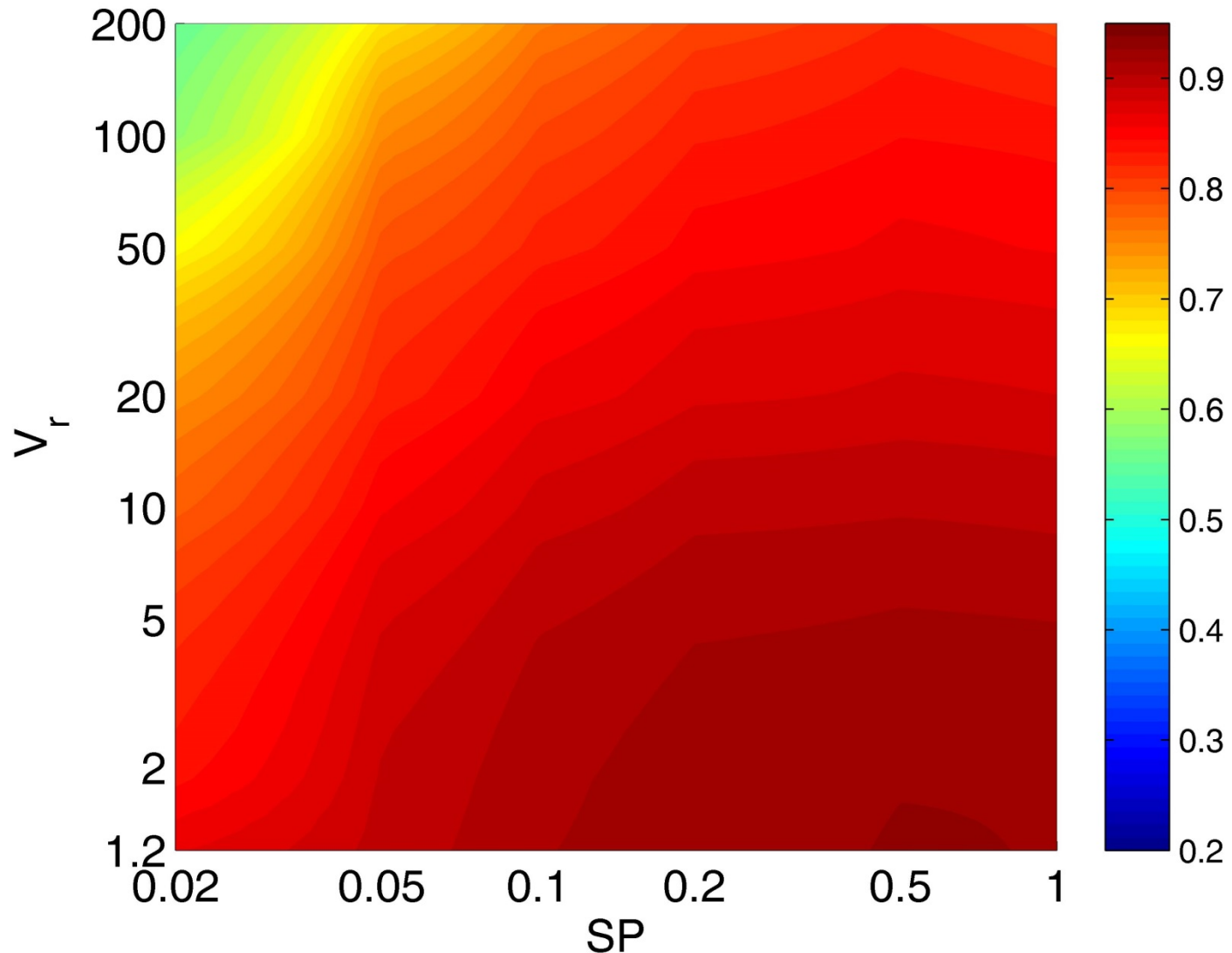




A new efficiency prediction map based on both  $V_r$  and  $SP$ , for optimized  $N_s$ ,  $D_s$

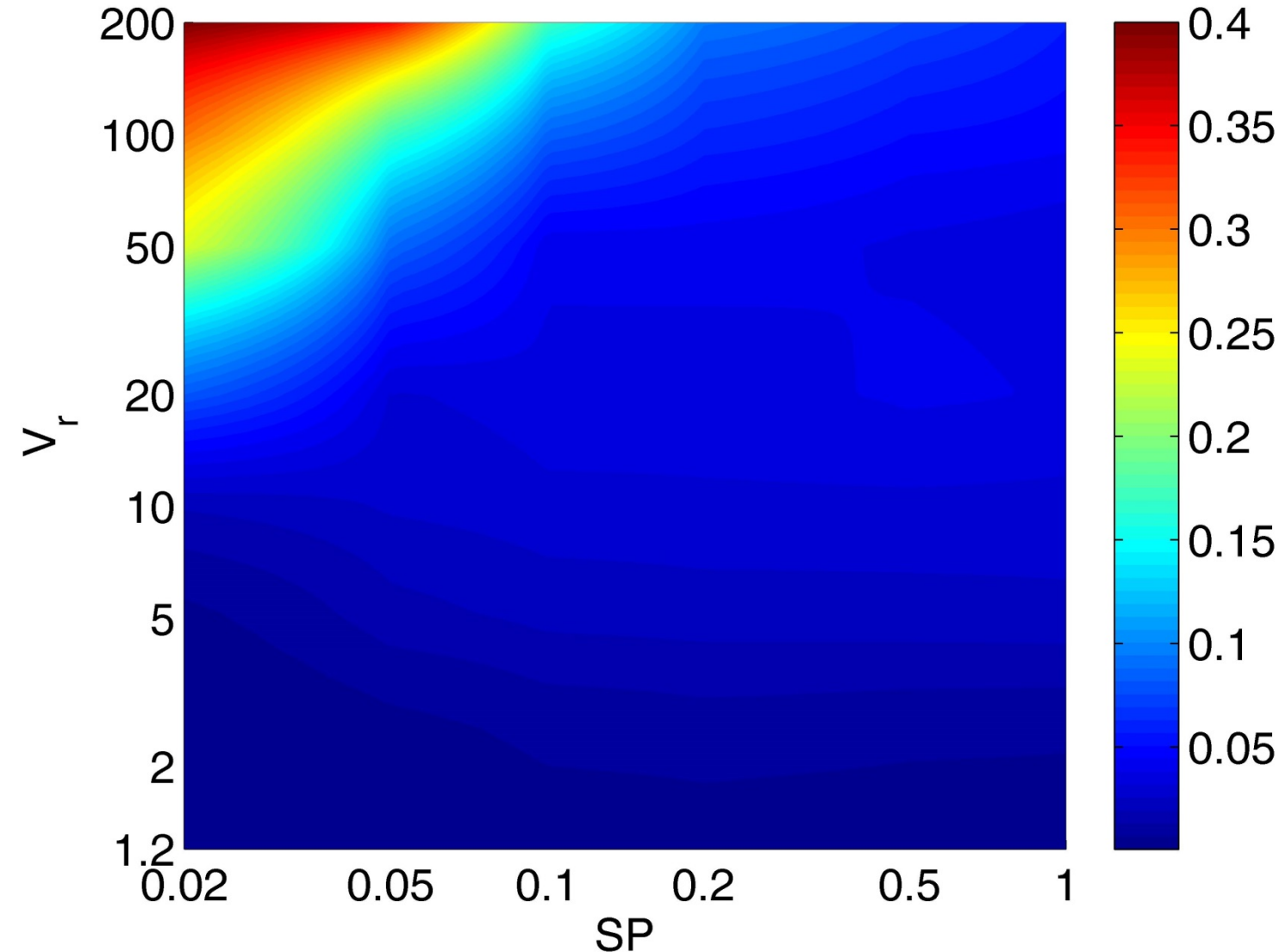
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## Two-stage turbine





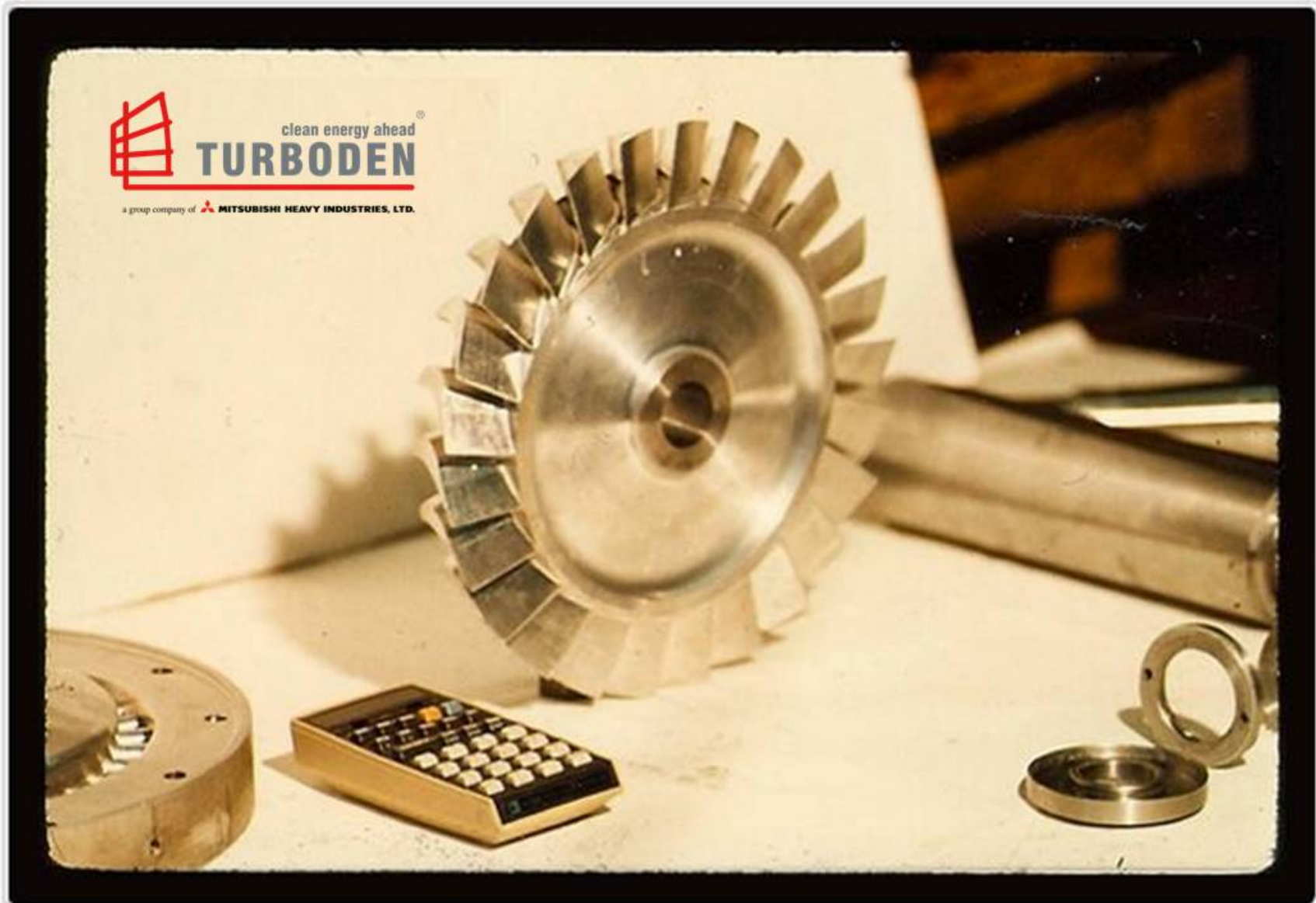
# Turbine efficiency improvement achievable by substituting a single stage with a two stages turbine 19





## First example (1978?): single-stage, 3000 rpm, 4 kWel

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## First example (1978?): single-stage, 3000 rpm, 3-4 kWel

Heat source: hot water (90-70°C)

Heat sink: cold water (15-25 °C)

Working fluid: C<sub>2</sub>Cl<sub>4</sub> (perchloroethylene), saturated cycle

- $T_{cr} = 121\text{ °C}$
- $M = 166\text{ kg/kmole}$

The first ORC built by Turboden

Demonstration that it is possible to design a high efficiency (>85%), low mechanical stress turbine, directly coupled to a 3000 rpm generator, even at very low power output





## Second example (1979): four stages axial flow turbine, 35 kWel<sup>22</sup>





## Second example (1979): four stages axial flow turbine, 35 kWel

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Heat source: Thermal oil (380-300°C) from CSP (parabolic through)

Heat sink: water (25-32°C)

Working fluid: Flutec PP3 (C8F16) recuperated cycle

- $T_{cr} = 515\text{ °C}$
- $M = 400\text{ kg/kmole}$

4 stages:

- first stage impulse, partial admission
- second stage shrouded (low blade height)
- third and fourth stages reaction stages, untwisted blades

Demonstration that it is possible to design a high efficiency (>85%), low mechanical stress turbine, directly coupled to a 3000 rpm generator, even for very high expansion ratio



Bado G., Tomei G., Angelino G., Gaia M., Macchi E. "THE ANSAL-DO 35 kW SOLAR POWER SYSTEM", Proceedings of International Solar Energy Society (ISES) Congress, Atlanta (USA), in "SUN II" Vol. 2, pp. 1090-1094, Pergamon Press, May 1979. 24







## Third example (2012): single-stage axial-flow turbine, R-134a 500 kWel (see ENEL presentation, this congress)

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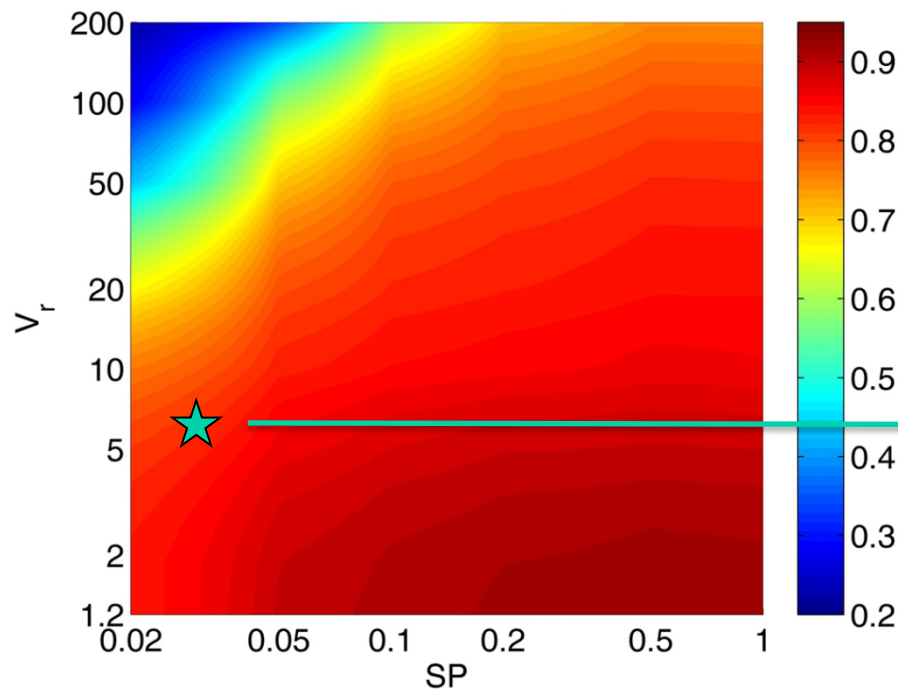


## Third example (2012): single-stage axial-flow turbine, R-134a, 500 kWel (see ENEL presentation, this congress)

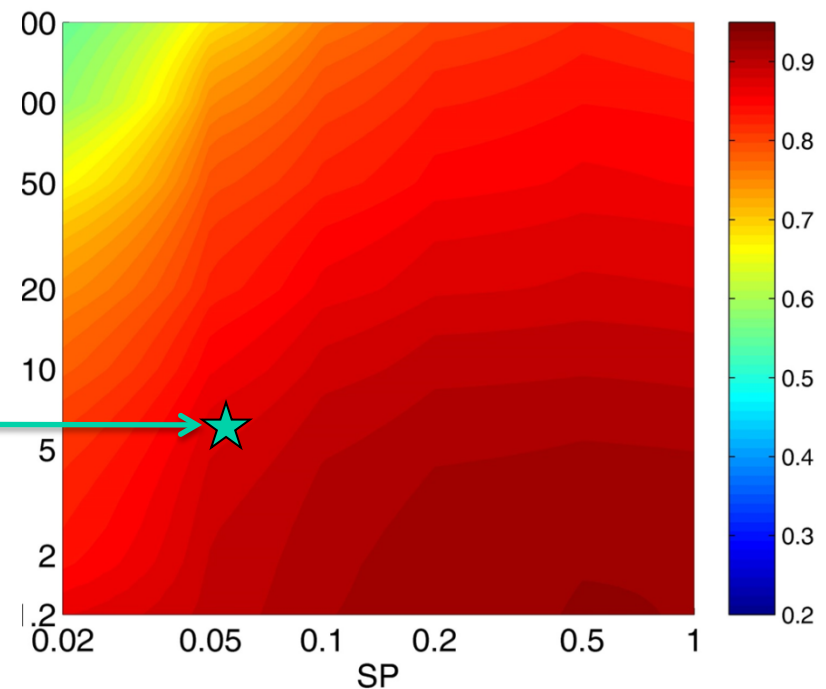
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- The test turbine was a single-stage, low  $N_s$ , SP axial turbine (500 kW)
- The scaled-up turbine will be a two-stage, high efficiency axial turbine (10 MW)

### Single-stage turbine



### Two-stage turbine







**Fourth example: 1000 kWel, 3 stages out-flow, working fluid: Flutec PP1, hot source: hot water (170 °C) cold sink: ambient air**

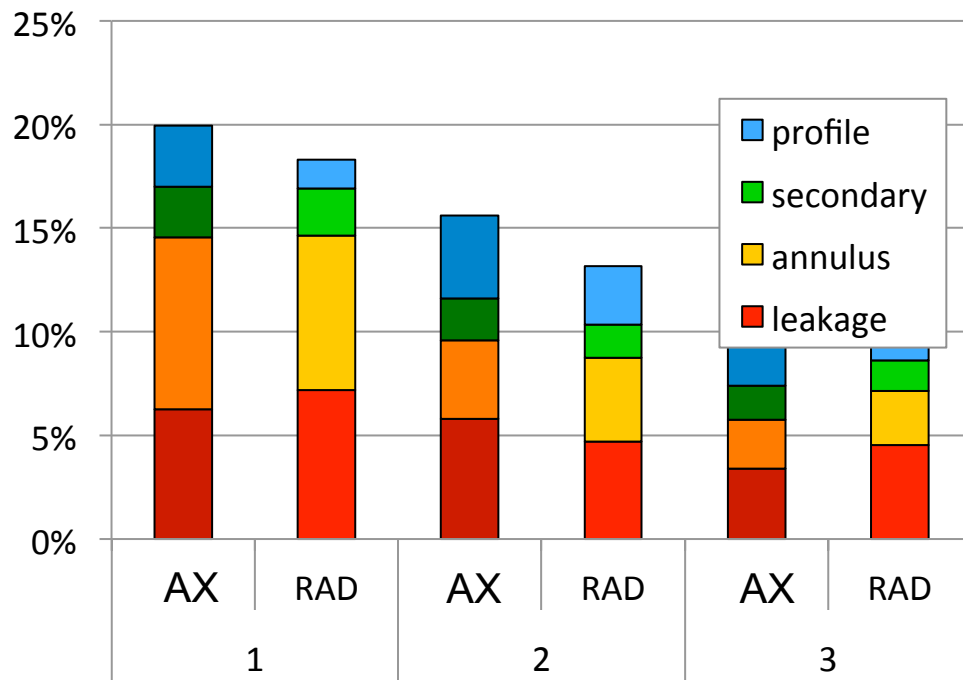
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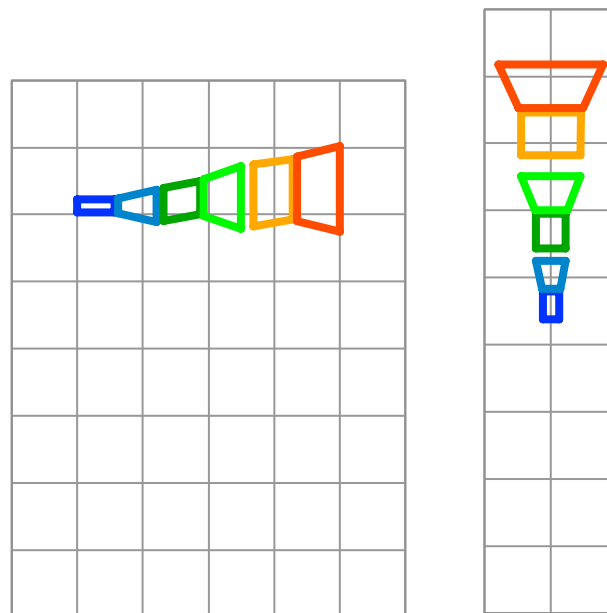
# RADIAL OUTFLOW vs AXIAL TURBINE

## Losses breakdown



$\Delta h$	AX		RAD	
1	31.9%	24.9%	79.3%	81.3%
2	31.9%	32.5%	84.1%	86.4%
3	36.2%	42.7%	85.5%	89.1%

$\eta$	AX		RAD	
1	79.3%	81.3%	84.1%	86.4%
2	84.1%	86.4%	85.5%	89.1%
3	85.5%	89.1%		



**Radial** vs Axial

**Efficiency  
+ 4.14%**

For the same ORC



**Fourth example: 1000 kWel, 3 stages out-flow, working fluid: Flutec PP1, hot source: hot water (170 °C) cold sink: ambient air**

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## Fifth example: 1 MWel, 4 stages outflow, working fluid: hydrocarbon

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**THANK YOU FOR YOUR ATTENTION !**