

Influence of Molecular Complexity on Nozzle Design for an Organic Vapor Wind Tunnel



A. Guardone, Aerospace Eng. Dept., PoliMI
A. Spinelli, V. Dossena, Energy Dept., PoliMI
V. Vandecaeter, Aerospace Eng., TUDelft

Motivation & Current Activities

Motivation of the proposed work:

Improvement of the performances of Organic Rankine Cycles (ORC) via better turbine design calls for experimental studies on ORC turbine flows

TROVA@PoliMI

- is designed to provide experimental data for flows typical of ORC turbine blade passages
- is a blow-down facility; expansion occurs through a **test section**: straight axis, planar, convergent-divergent nozzle
- Working fluid: siloxane MDM

Motivation & Current Activities

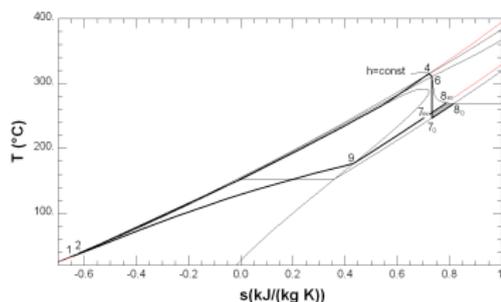
Motivation of the proposed work:

Improvement of the performances of Organic Rankine Cycles (ORC) via better turbine design calls for experimental studies on ORC turbine flows

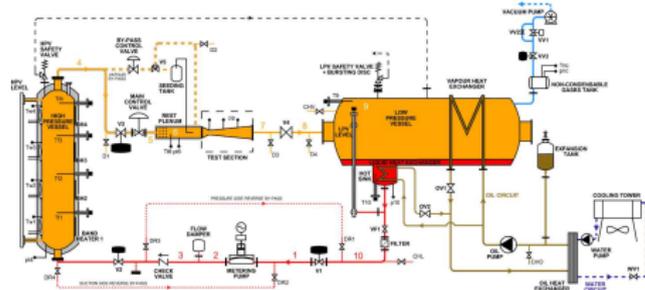
TROVA@PoliMI

- is designed to provide experimental data for flows typical of ORC turbine blade passages
- is a blow-down facility; expansion occurs through a **test section**: straight axis, planar, convergent-divergent nozzle
- Working fluid: siloxane MDM

TROVA@Polimi

*TMD Cycle*

- 4 - High Pressure Vessel
- 6 - Nozzle Inlet
- 7 - Nozzle Outlet
- 8 - Low Pressure Vessel



Presentation at 11.20 Senaatszaal...

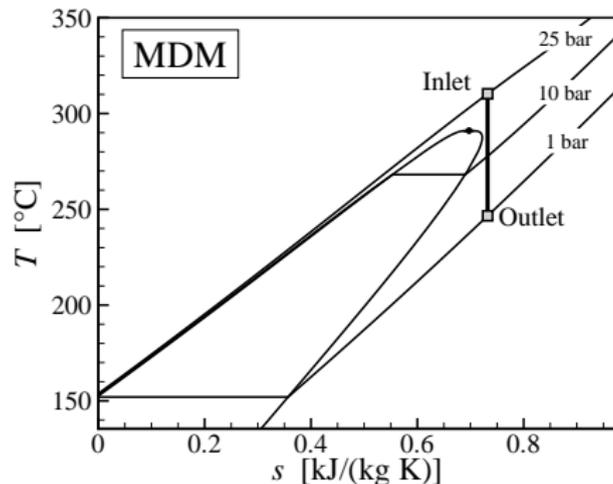
Design issue

The understanding of the gasdynamics of supercritical and close-to-critical flows is incomplete!

Nozzle design for ORC applications

Expansion occurs in highly non-ideal gas conditions

- Real-gas thermodynamic models
- High compressibility
- Non-ideal dependence of the speed of sound c on specific volume v at constant T



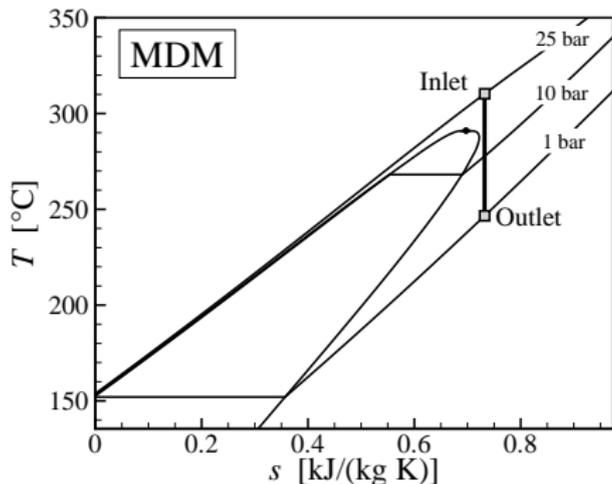
Dense gas dynamics

Nozzle design for ORC applications

Expansion occurs in highly non-ideal gas conditions

- Real-gas thermodynamic models
- High compressibility
- Non-ideal dependence of the speed of sound c on specific volume v at constant T

Dense gas dynamics



Fundamental derivative of gasdynamics

Phil Thompson, J. Fluids Mech. 1971

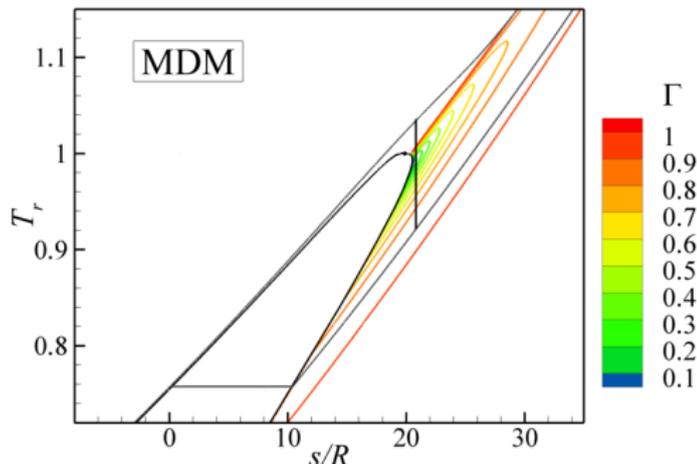
Fundamental derivative Γ

$$\Gamma = 1 + \frac{\rho}{c} \left(\frac{\partial c}{\partial \rho} \right)_s$$

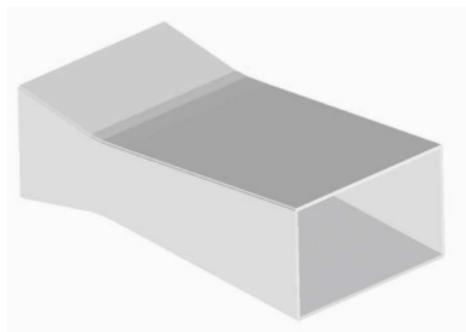
c sound speed

ρ density

s entropy p.u.m.



Goal of the research



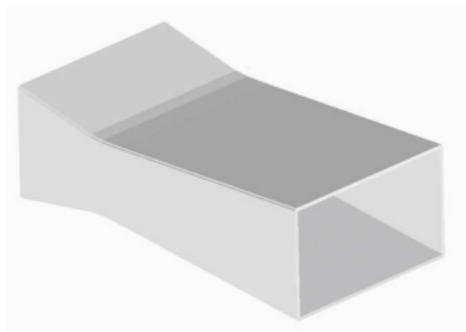
Goal of the research

To design the divergent section of subsonic-supersonic nozzles operating in the dense gas regime

Assumptions

Flow is two-dimensional, flow is expanding from uniform reservoir conditions into uniform ambient conditions, high-Reynolds number flow, no flow separation, no shock waves, adiabatic walls

Goal of the research



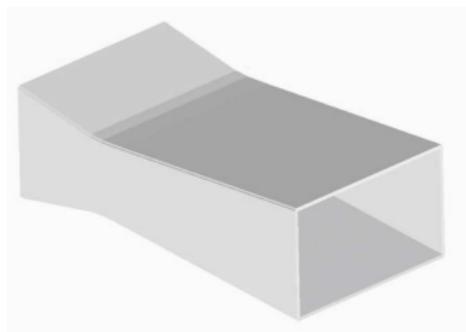
Goal of the research

To design the divergent section of subsonic-supersonic nozzles operating in the dense gas regime

Assumptions

Flow is two-dimensional, flow is expanding from uniform reservoir conditions into uniform ambient conditions, high-Reynolds number flow, no flow separation, no shock waves, adiabatic walls

Goal of the research



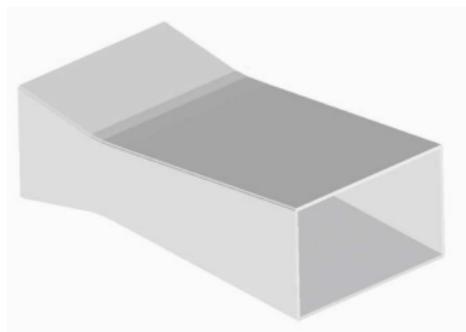
Goal of the research

To design the divergent section of subsonic-supersonic nozzles operating in the dense gas regime

Assumptions

Flow is two-dimensional, flow is expanding from uniform reservoir conditions into uniform ambient conditions, high-Reynolds number flow, no flow separation, no shock waves, adiabatic walls

Goal of the research



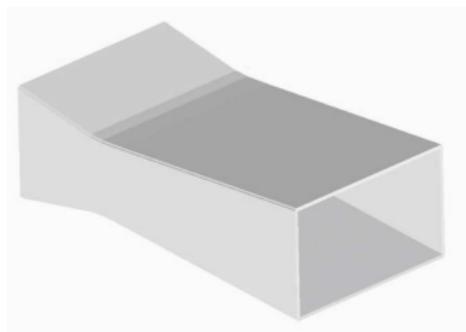
Goal of the research

To design the divergent section of subsonic-supersonic nozzles operating in the dense gas regime

Assumptions

Flow is two-dimensional, flow is expanding from uniform reservoir conditions into uniform ambient conditions, high-Reynolds number flow, no flow separation, no shock waves, adiabatic walls

Goal of the research



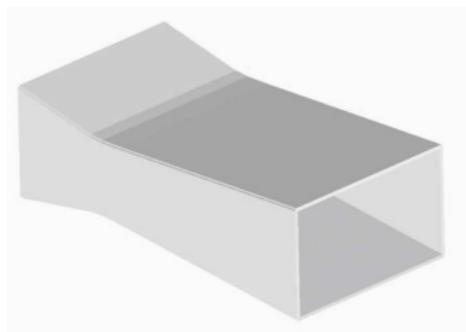
Goal of the research

To design the divergent section of subsonic-supersonic nozzles operating in the dense gas regime

Assumptions

Flow is two-dimensional, flow is expanding from uniform reservoir conditions into uniform ambient conditions, high-Reynolds number flow, no flow separation, no shock waves, adiabatic walls

Goal of the research



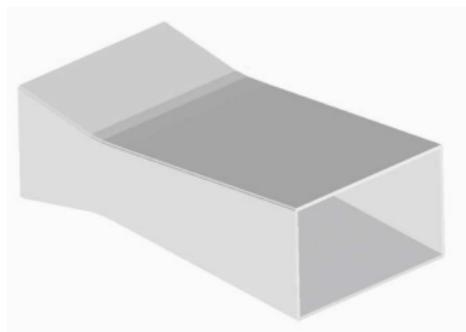
Goal of the research

To design the divergent section of subsonic-supersonic nozzles operating in the dense gas regime

Assumptions

Flow is two-dimensional, flow is expanding from uniform reservoir conditions into uniform ambient conditions, high-Reynolds number flow, no flow separation, no shock waves, *adiabatic walls*

Goal of the research



Goal of the research

To design the divergent section of subsonic-supersonic nozzles operating in the dense gas regime

Assumptions

Flow is two-dimensional, flow is expanding from uniform reservoir conditions into uniform ambient conditions, high-Reynolds number flow, no flow separation, no shock waves, adiabatic walls

Mathematical model

Full potential equation

Compressible non-viscous isentropic irrotational flow

$$\left(\Phi_x^2 - c^2\right) \Phi_{xx} + 2 \Phi_x \Phi_y \Phi_{xy} + \left(\Phi_y^2 - c^2\right) \Phi_{yy} = 0$$

with $\Phi \in \mathbb{R}$, $u = \Phi_x$ and $v = \Phi_y$ flow velocities, $w^2 = u^2 + v^2$.

Thermodynamic closure

$$c = c(s, h) = c(s_r, h_r - w^2/2) \quad ?$$

StanMix and RefProp libraries in FluidProp:

- Stryjek-Vera Peng-Robinson cubic EOS (PRSV)
- Span Wagner multiparameter EOS (SW)

Mathematical model

Full potential equation

Compressible non-viscous isentropic irrotational flow

$$\left(\Phi_x^2 - c^2\right) \Phi_{xx} + 2 \Phi_x \Phi_y \Phi_{xy} + \left(\Phi_y^2 - c^2\right) \Phi_{yy} = 0$$

with $\Phi \in \mathbb{R}$, $u = \Phi_x$ and $v = \Phi_y$ flow velocities, $w^2 = u^2 + v^2$.

Thermodynamic closure

$$c = c(s, h) = c(s_r, h_r - w^2/2) \quad ?$$

StanMix and RefProp libraries in FluidProp:

- Stryjek-Vera Peng-Robinson cubic EOS (PRSV)
- Span Wagner multiparameter EOS (SW)

Mathematical model

Full potential equation

Compressible non-viscous isentropic irrotational flow

$$\left(\Phi_x^2 - c^2\right) \Phi_{xx} + 2 \Phi_x \Phi_y \Phi_{xy} + \left(\Phi_y^2 - c^2\right) \Phi_{yy} = 0$$

with $\Phi \in \mathbb{R}$, $u = \Phi_x$ and $v = \Phi_y$ flow velocities, $w^2 = u^2 + v^2$.

Thermodynamic closure

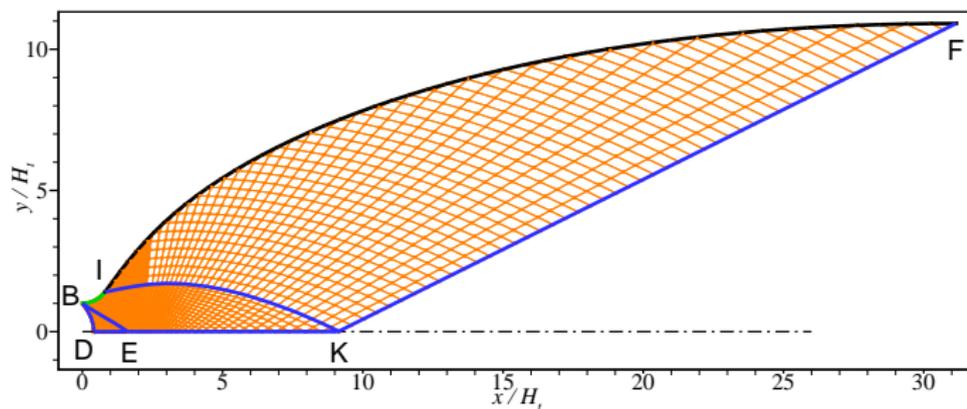
$$c = c(s, h) = c(s_r, h_r - w^2/2) \quad ?$$

StanMix and RefProp libraries in FluidProp:

- Stryjek-Vera Peng-Robinson cubic EOS (PRSV)
- Span Wagner multiparameter EOS (SW)

Design procedure

Method Of Characteristics (MOC) (Zucrow & Hoffman, 1977)



Initial data (BD)

Sauer (1947) scheme

$$2\Gamma^* \phi_x \phi_{xx} - \phi_{yy} = 0$$

Kernel region (BIKD)

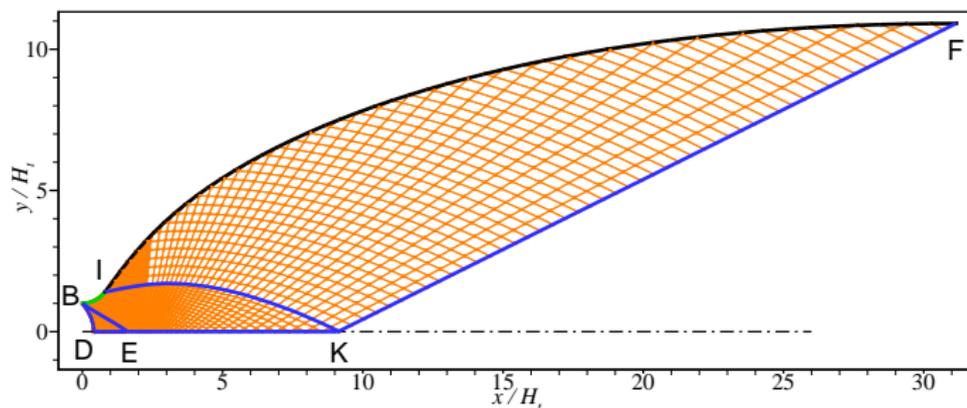
Direct MOC from
initial data line BD

Turning region (IKF)

Inverse MOC from exit
characteristic KF

Design procedure

Method Of Characteristics (MOC) (Zucrow & Hoffman, 1977)



Initial data (BD)

Sauer (1947) scheme

$$2\Gamma^* \phi_x \phi_{xx} - \phi_{yy} = 0$$

Kernel region (BIKD)

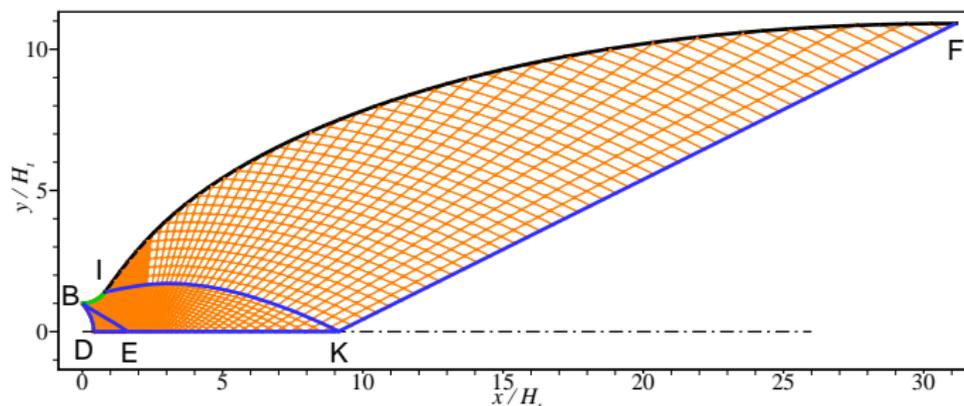
Direct MOC from
initial data line BD

Turning region (IKF)

Inverse MOC from exit
characteristic KF

Design procedure

Method Of Characteristics (MOC) (Zucrow & Hoffman, 1977)



Initial data (BD)

Sauer (1947) scheme

$$2\Gamma^* \phi_x \phi_{xx} - \phi_{yy} = 0$$

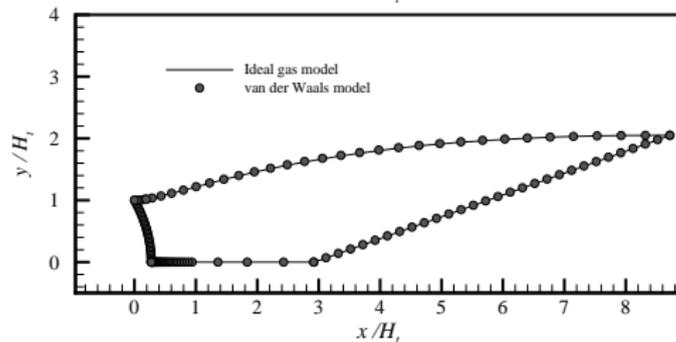
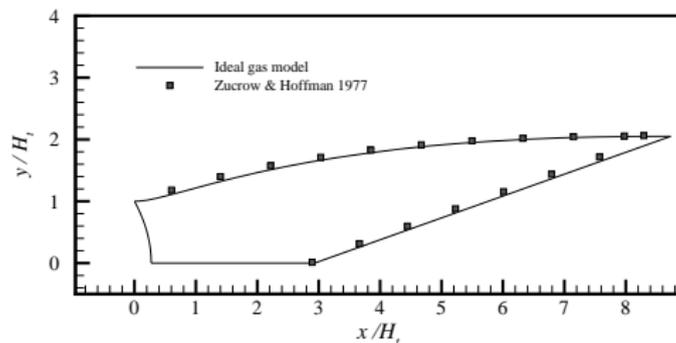
Kernel region (BIKD)

Direct MOC from
initial data line BD

Turning region (IKF)

Inverse MOC from exit
characteristic KF

Recovery of perfect gas results



Perfect gas results

Diatomic nitrogen
dilute conditions

Nozzle design for MDM

Reservoir conditions

$$P_0 = 25 \text{ bar}$$

$$T_0 = 310.3 \text{ }^\circ\text{C}$$

Expansion ratio

$$\beta = 25$$

Design conditions

Exit Mach number

$$M_d = 2.25$$

Velocity vector parallel
to x axis

Nozzle design for MDM

Reservoir conditions

$$P_0 = 25 \text{ bar}$$

$$T_0 = 310.3 \text{ }^\circ\text{C}$$

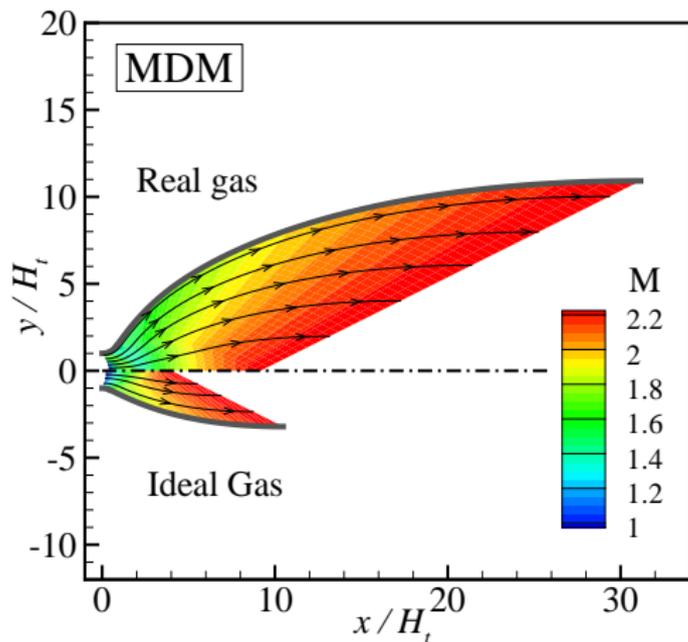
Expansion ratio

$$\beta = 25$$

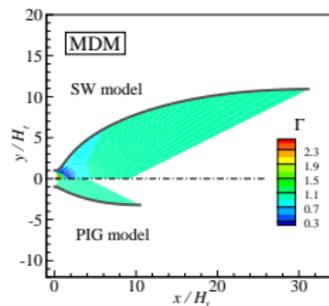
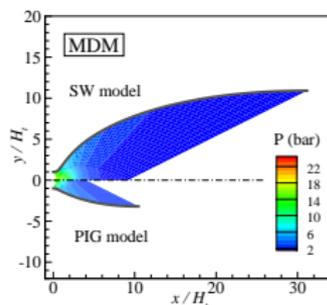
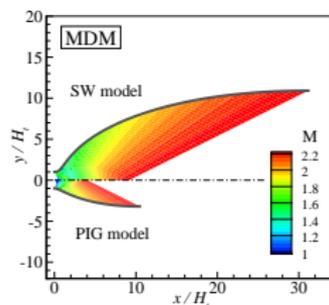
Design conditions

Exit Mach number

$$M_d = 2.25$$

Velocity vector parallel
to x axis

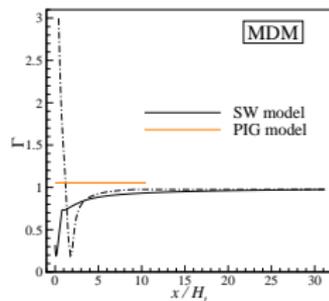
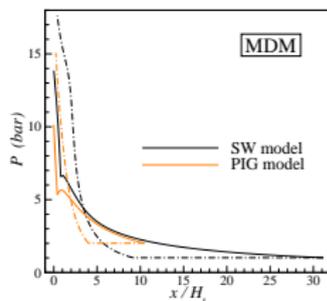
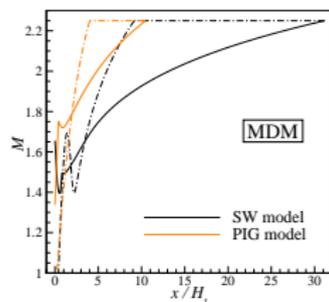
Nozzle design for MDM



$$\frac{dM}{dx} = \frac{1 + (\Gamma - 1)M^2}{M^2 - 1} \frac{M}{H} \frac{dH}{dx}$$

$$\frac{dP}{dx} = \frac{\rho u^2}{P} \frac{1}{M^2 - 1} \frac{P}{H} \frac{dH}{dx}$$

$$\Gamma = 1 + \frac{\rho}{c} \left(\frac{\partial c}{\partial \rho} \right)_s$$



Nozzle design for different fluids

Fluids

D₄, D₅, D₆,
MM, MDM, MD₂M
R245fa, Toluene,
Ammonia

Nozzle design for different fluids

Fluids

D₄, D₅, D₆,
MM, MDM, MD₂M
R245fa, Toluene,
Ammonia

Warning

Thermal decomposition!!!

Nozzle design for different fluids

Fluids

D₄, D₅, D₆,
MM, MDM, MD₂M
R245fa, Toluene,
Ammonia

Warning

Thermal decomposition!!!

Design parameters

$$P_0 = 0.78P_c$$

$$T_0 = 0.975T_c$$

$$\beta = 25 \rightarrow P_d = 0.031P_c$$

Nozzle design for different fluids

Fluids

D₄, D₅, D₆,
MM, MDM, MD₂M
R245fa, Toluene,
Ammonia

Warning

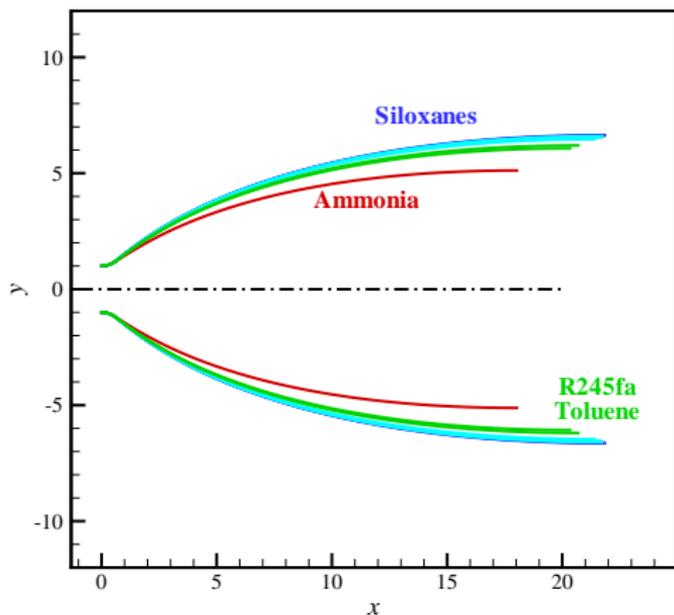
Thermal decomposition!!!

Design parameters

$$P_0 = 0.78P_c$$

$$T_0 = 0.975T_c$$

$$\beta = 25 \rightarrow P_d = 0.031P_c$$



Nozzle design for different fluids

Fluids

D₄, D₅, D₆,
MM, MDM, MD₂M
R245fa, Toluene,
Ammonia

Warning

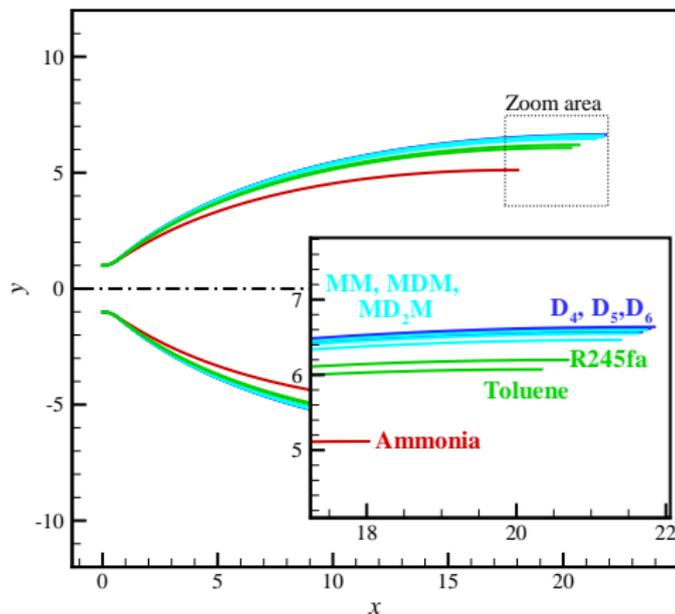
Thermal decomposition!!!

Design parameters

$$P_0 = 0.78P_c$$

$$T_0 = 0.975T_c$$

$$\beta = 25 \rightarrow P_d = 0.031P_c$$



Conclusions

- A nozzle design tool for dense gases was developed and validated against ideal gas results using the the cubic PRSV EoS and the multi-parameter Span-Wagner EoS in FluidProp
- If the expansion process occurs in region where Γ is less than its dilute-gas value, then resulting nozzles are longer, in accordance with the one-dimensional theory.
- For increasing molecular complexity of the fluid, Γ decreases and the nozzle length increases.
- Caution: normalized mass flow varies dramatically for the diverse operating conditions

Thank you!