

Influence of Molecular Complexity on Nozzle Design for an Organic Vapor Wind Tunnel

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Motivation & Current Activities

Motivation of the proposed work:

Improvement of the performances of Organic Rankine Cycles (ORC) via better turbine design calls for experimental studies on ORC turbine flows

TROVA@PoliMI

- is designed to provide experimental data for flows typical of ORC turbine blade passages
- is a blow-down facility; expansion occurs through a **test section**: straight axis, planar, convergent-divergent nozzle
- Working fluid: siloxane MDM

Motivation & Current Activities

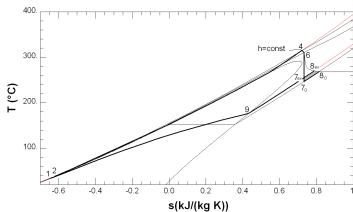
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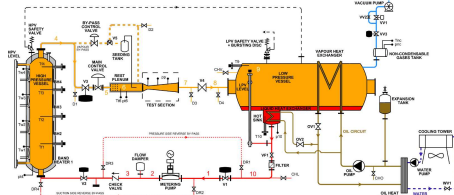
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*TMD Cycle*

- 4 - High Pressure Vessel
- 6 - Nozzle Inlet
- 7 - Nozzle Outlet
- 8 - Low Pressure Vessel

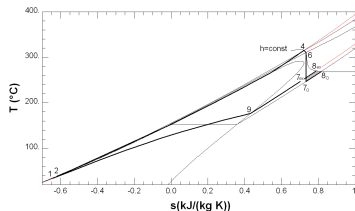
Design issue

The understanding of the gasdynamics of supercritical and close-to-critical flows is incomplete!



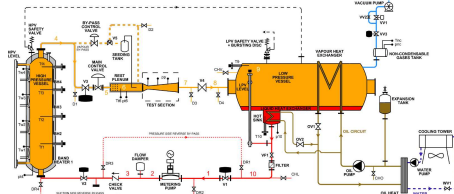
Presentation at 11.20 Senaatszaal...

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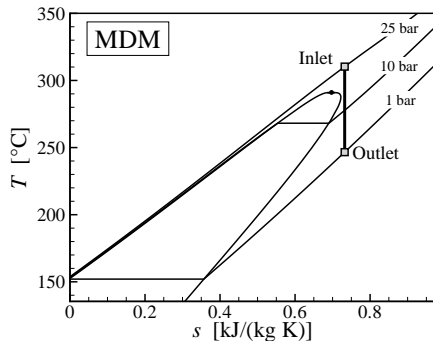
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Nozzle design for ORC applications

Expansion occurs in highly non-ideal gas conditions

- Real-gas thermodynamic models
- High compressibility
- Non-ideal dependence of the speed of sound c on specific volume v at constant T

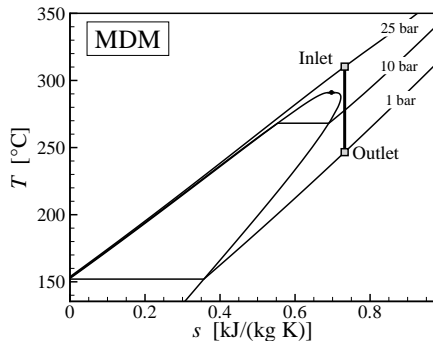


Dense gas dynamics

Nozzle design for ORC applications

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Dense gas dynamics

Fundamental derivative of gasdynamics

Phil Thompson, J. Fluids Mech. 1971

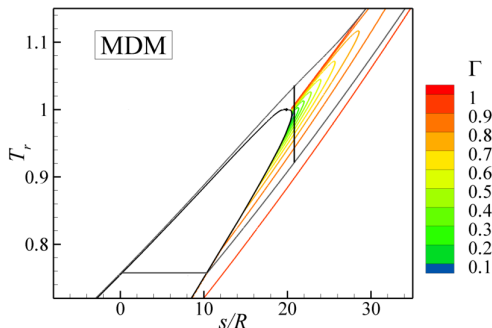
Fundamental derivative Γ

$$\Gamma = 1 + \frac{\rho}{c} \left(\frac{\partial c}{\partial \rho} \right)_s$$

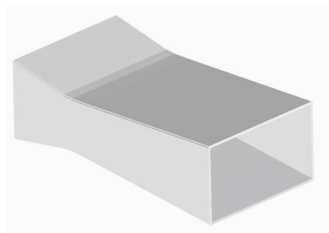
c sound speed

ρ density

s entropy p.u.m.



Goal of the research



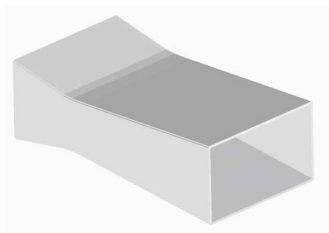
Goal of the research

To design the divergent section of subsonic-supersonic nozzles operating in the dense gas regime

Assumptions

Flow is two-dimensional, flow is expanding from uniform reservoir conditions into uniform ambient conditions, high-Reynolds number flow, no flow separation, no shock waves, adiabatic walls

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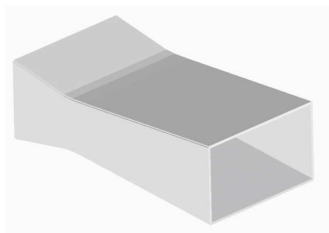
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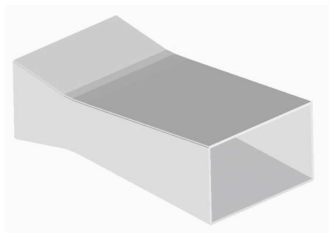
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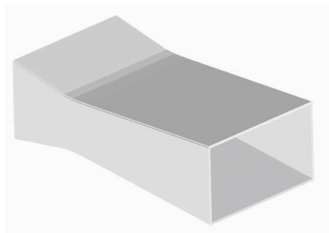
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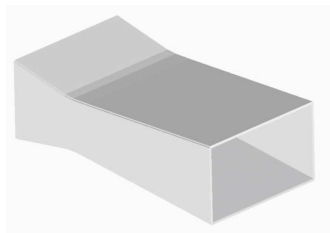
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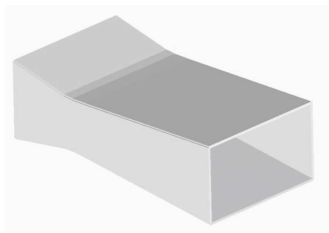
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Mathematical model

Full potential equation

Compressible non-viscous isentropic irrotational flow

$$(\Phi_x^2 - c^2) \Phi_{xx} + 2 \Phi_x \Phi_y \Phi_{xy} + (\Phi_y^2 - c^2) \Phi_{yy} = 0$$

with $\Phi \in \mathbb{R}$, $u = \Phi_x$ and $v = \Phi_y$ flow velocities, $w^2 = u^2 + v^2$.

Thermodynamic closure

$$c = c(s, h) = c(s_r, h_r - w^2/2) \quad ?$$

StanMix and RefProp libraries in FluidProp:

- Stryjek-Vera Peng-Robinson cubic EOS (PRSV)
- Span Wagner multiparameter EOS (SW)

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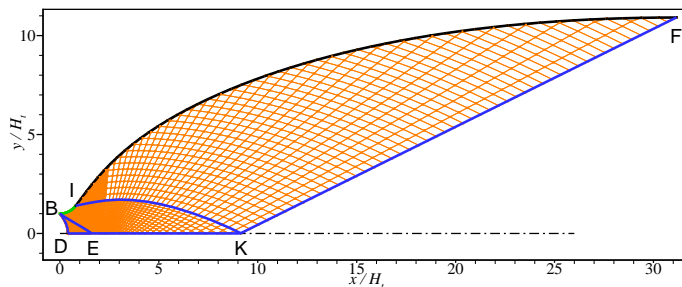
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Design procedure

Method Of Characteristics (MOC) (Zucrow & Hoffman, 1977)



Initial data (BD)

Sauer (1947) scheme
 $2\Gamma^* \phi_x \phi_{xx} - \phi_{yy} = 0$

Kernel region (BIKD)

Direct MOC from
 initial data line BD

Turning region (IKF)

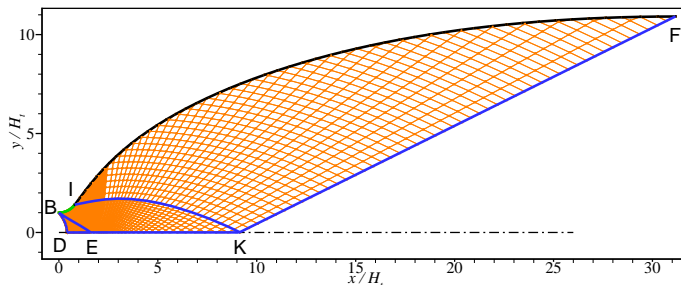
Inverse MOC from exit
 characteristic KF

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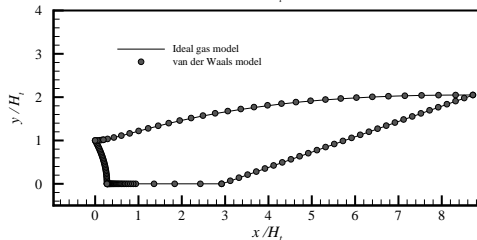
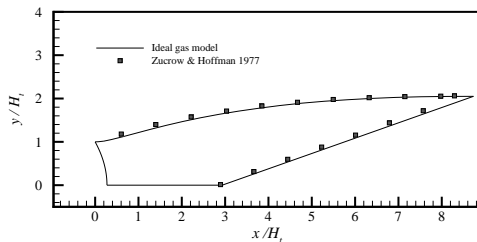
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Recovery of perfect gas results



Perfect gas results

Diatomic nitrogen
dilute conditions

Nozzle design for MDM

Reservoir conditions

$$P_0 = 25 \text{ bar}$$

$$T_0 = 310.3 \text{ }^\circ\text{C}$$

Expansion ratio

$$\beta = 25$$

Design conditions

Exit Mach number

$$M_d = 2.25$$

Velocity vector parallel
to x axis

Nozzle design for MDM

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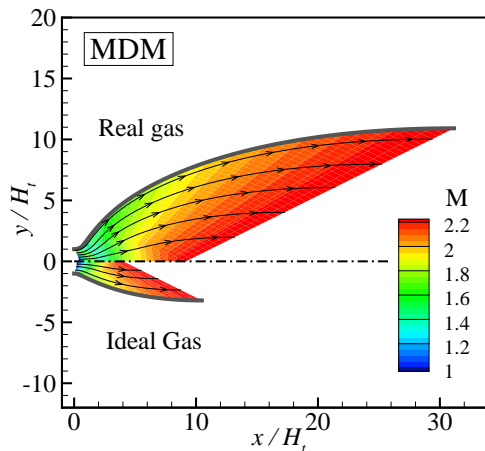
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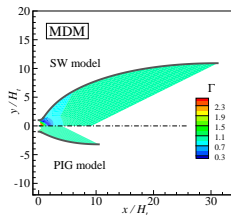
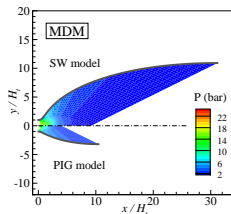
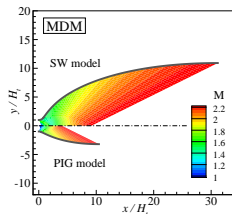
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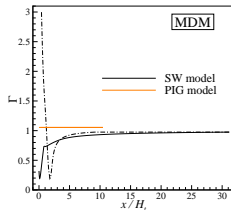
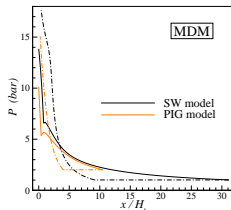
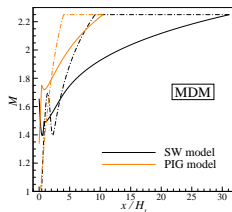
Nozzle design for MDM



$$\frac{dM}{dx} = \frac{1 + (\Gamma - 1)M^2}{M^2 - 1} \frac{M}{H} \frac{dH}{dx}$$

$$\frac{dP}{dx} = \frac{\rho u^2}{P} \frac{1}{M^2 - 1} \frac{P}{H} \frac{dH}{dx}$$

$$\Gamma = 1 + \frac{\rho}{c} \left(\frac{\partial c}{\partial \rho} \right)_s$$



Nozzle design for different fluids

Fluids

D₄, D₅, D₆,
MM, MDM, MD₂M
R245fa, Toluene,
Ammonia

Nozzle design for different fluids

Fluids

D₄, D₅, D₆,
MM, MDM, MD₂M
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Warning

Thermal decomposition!!!

Nozzle design for different fluids

Fluids

D₄, D₅, D₆,
MM, MDM, MD₂M
R245fa, Toluene,
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Thermal decomposition!!!

Design parameters

$$P_0 = 0.78P_c$$

$$T_0 = 0.975T_c$$

$$\beta = 25 \rightarrow P_d = 0.031P_c$$

Nozzle design for different fluids

Fluids

D₄, D₅, D₆,
MM, MDM, MD₂M
R245fa, Toluene,
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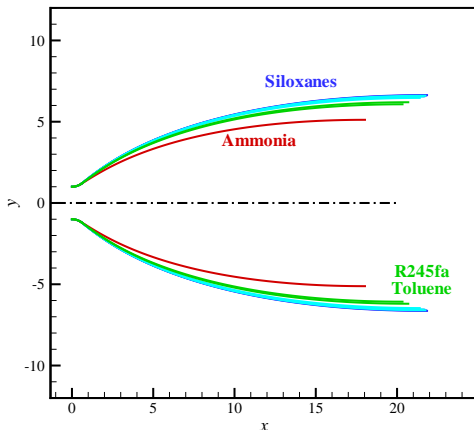
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Nozzle design for different fluids

Fluids

D_4 , D_5 , D_6 ,
MM, MDM, MD_2M
R245fa, Toluene,
Ammonia

Warning

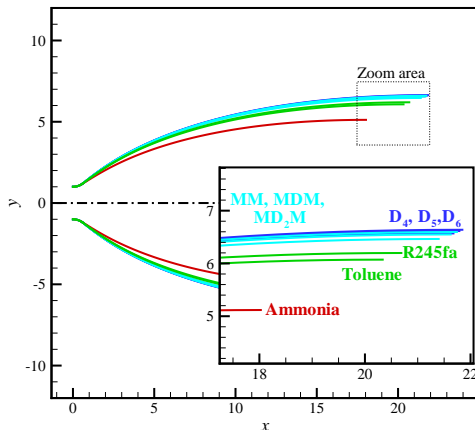
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Conclusions

- A nozzle design tool for dense gases was developed and validated against ideal gas results using the cubic PRSV EoS and the multi-parameter Span-Wagner EoS in FluidProp
- If the expansion process occurs in region where Γ is less than its dilute-gas value, then resulting nozzles are longer, in accordance with the one-dimensional theory.
- For increasing molecular complexity of the fluid, Γ decreases and the nozzle length increases.
- Caution: normalized mass flow varies dramatically for the diverse operating conditions

Thank you!